## AUIS ENGR 352 (Thermodynamics), Assignment II

Submission deadline: ${ }^{1}$ March 11, 2018
Tutorial discussion: March 27 and 29, 2018

1) Consider the following reversible cycle with the working fluid propane, to be approximated here as an ideal gas with the specific isochoric heat capacity $c_{v}=(\partial u / \partial T)_{v}=5.50 \mathrm{R}$ :

- Transition $1 \rightarrow 2$ : Isobaric expansion, $p_{1}=p_{2}=40 \mathrm{kPa}$, to the volume $v_{2}=120 \mathrm{I} \mathrm{mol}^{-1}$.
- Transition $2 \rightarrow 3$ : Isochoric cooling until the pressure $p_{3}=25 \mathrm{kPa}$ is reached.
- Transition $3 \rightarrow 1$ : Adiabatic compression from $p_{3}=25 \mathrm{kPa}$ to $p_{1}=40 \mathrm{kPa}$.
a) Draw a $p$-v diagram for this process. Is it a power or refrigeration cycle?
b) Determine the net power received by the gas and the net heat transferred to the gas per time for a (molar) substance flow rate of $2.7 \mathrm{~mol} \mathrm{~s}^{-1}$. Pay attention to the signs. To the fluid: positive; from the fluid: negative. The molar mass of propane is $M=44.10 \mathrm{~g} \mathrm{~mol}^{-1}$.

2) Going through an adiabatic nozzle that operates in a steady state, ethane, to be treated here as an ideal gas with the specific isobaric heat capacity $c_{p}=1.333 \mathrm{~kJ} \mathrm{~K}^{-1} \mathrm{~kg}^{-1}$, is accelerated from its initial velocity, at the inlet, to an outlet velocity of $126 \mathrm{~m} \mathrm{~s}^{-1}$. From inlet to outlet, the temperature decreases by $T_{\text {out }}-T_{\text {in }}=-3.9 \mathrm{~K}$.
Determine the velocity at the inlet. For an ideal gas, the speed of sound is $\mathcal{V}_{s}=(\kappa p v / M)^{1 / 2}$, where $\kappa=1.262$ is the polytropic exponent of ethane at the conditions in the nozzle, $p$ is the pressure, $v$ is the molar volume, and $M=30.07 \mathrm{~g} \mathrm{~mol}^{-1}$ is the molar mass of ethane.
3) R134a enters an adiabatic diffuser, which operates in a steady state, at the temperature $20^{\circ} \mathrm{C}$ and the velocity $270 \mathrm{~m} \mathrm{~s}^{-1}$, in a vapor-liquid coexistence state with the quality $90 \%$, and it leaves the diffuser with $70 \mathrm{~m} \mathrm{~s}^{-1}$ at 300 kPa . Use the $\log p$-h diagram from the lecture to determine the temperature difference between the inlet and the outlet.
4) Isobaric heat transfer is characterized by the specific isobaric heat capacity $c_{p}=(\partial h / \partial T)_{p}$. Liquid phase and supercritical data for refrigerant R124 at $p=8700 \mathrm{kPa}$ include:

$$
\begin{array}{llll}
p=8700 \mathrm{kPa} \text { and } T=340 \mathrm{~K}: & v=793.5 \mathrm{ml} \mathrm{~kg}^{-1} & u=270.1 \mathrm{~kJ} \mathrm{~kg}^{-1} & c_{v}=808.4 \mathrm{~J} \mathrm{~K}^{-1} \mathrm{~kg}^{-1} \\
p=8700 \mathrm{kPa} \text { and } T=360 \mathrm{~K}: & v=842.6 \mathrm{ml} \mathrm{~kg} \\
p=8700 \mathrm{kPa} \text { and } T=380 \mathrm{~K}: & v=906.1 \mathrm{ml} \mathrm{~kg}^{-1} & u=293.7 \mathrm{~kJ} \mathrm{~kg}^{-1} & c_{v}=830.9 \mathrm{~J} \mathrm{~K}^{-1} \mathrm{~kg}^{-1} \\
p=8700 \mathrm{kPa} \text { and } T=400 \mathrm{~K}: & v=994.2 \mathrm{ml} \mathrm{~kg}^{-1} & u=344.3 \mathrm{~kJ} \mathrm{~kg}^{-1} & c_{v}=854.7 \mathrm{~J} \mathrm{~K}^{-1} \mathrm{~kg}^{-1} \\
c_{v}=880.3 \mathrm{~J} \mathrm{~K}^{-1} \mathrm{~kg}^{-1}
\end{array}
$$

Interpolate the specific isobaric heat capacity of liquid R124 at $p=8700 \mathrm{kPa}$ and $T=350 \mathrm{~K}$.
5) A refrigerator with the coefficient of performance $\varepsilon=4$ uses ammonia as working fluid to transfer heat from a cold region at $-11^{\circ} \mathrm{C}$ to a hot region at $44^{\circ} \mathrm{C}$.
a) Is the second law satisfied? Assuming reversible heat transfer, calculate the total entropy change for the two regions while 10 kJ of heat are taken in from the cold region.
b) Is the second law satisfied if the two temperatures and the working fluid ammonia remain the same, but the coefficient of performance is specified as $\varepsilon=6$ ?
6) A piston-cylinder device, with a constant pressure of $p=40 \mathrm{kPa}$ inside, contains $\mathrm{m}=90 \mathrm{~g}$ of water under vapor-liquid equilibrium conditions (both in the initial and the final state). Part of the liquid evaporates reversibly, and the volume increases by $140 \%$. In the final state, $m^{\prime}=78 \mathrm{~g}$ of the water are liquid, while the remaining $m^{\prime \prime}=12 \mathrm{~g}$ are steam.
How much heat is transferred to the fluid, and how much work is done by the fluid? Use the available resources to obtain the vapor-liquid equilibrium properties of water at 40 kPa .

[^0]
[^0]:    1 Each problem contributes up to one credit to the overall grade. Submissions, individually or in groups of two, can be handed in on March 11 (at lecture time only), or deposited in the B-F2-01 mailbox by March 10.

